



Scopus® doi

Journal of Vibration Engineering

ISSN:1004-4523

Registered



SCOPUS



GOOGLE SCHOLAR



DIGITAL OBJECT
IDENTIFIER (DOI)



IMPACT FACTOR 6.1



Our Website
www.jove.science

Extraction of Chemicals from the Bio-oil

Nishu¹, Nikita Goswami¹

¹University Institute of Biotechnology, Chandigarh University, Gharuan

nishu.uibt@cumail.in

Abstract

Bio-oil is an alternative liquid fuel, obtained from pyrolysis of biomass, which can be used for production of chemicals. Separation of chemicals from bio-oil helps improve the efficiency of bio-oil. Chemicals separated from bio-oil can be used as feedstocks in a biorefinery using different processes, which is an economical way to utilize bio-oil. The chemicals extracted from bio-oil can be used in agricultural, food or chemical industry, as nitrogen slow-releasing organic fertilizer, flavoring additives, de-icer agent and phenolic resins.

Keywords: *Bio-oil, chemicals, feedstocks, pyrolysis*

Introduction

The chemical composition of bio-oil is considerably totally different from that of crude oil fuels. It consists of various compounds derived from decomposition reactions of polyose, hemicellulose, and lignin. The chemical composition of bio-oil varies counting on the sort of biomass feedstock and also the operational parameters. usually speaking, bio-oil may be a mixture of water and complicated oxygen-rich organic compounds, together with most such styles of organic compounds, that is, alcohols, organic acids, ethers, esters, aldehydes, ketones, phenols, etc. Normally, the element distribution of bio-oil is also measured by GC-MS analysis. Crude bio-oil derived from lignocellulose may be a chromatic, viscous, however free-flowing liquid with a pungent odor. Crude bio-oil has associate degree gas content of 30–50 World Trade Center, leading to instability and an occasional heating worth (Oasmaa & C., 2001). The water content of bio-oil ranges from fifteen to fifty World Trade Center. The high water content of bio-oil derives from water within the feedstock and dehydration reactions throughout biomass shift (Bridgwater, 2012). Heating worth is a vital indicator for fuel oils. The heating worth of bio-oil is sometimes under twenty MJ/kg, abundant under that of heating oil. The high water content and gas content are 2 factors to blame for its low heating worth. The density of bio-oil derived from quick shift is at intervals the vary 1100–1300 kg/m³ (Adjaye et al., 1992). The hydrogen ion concentration worth of bio-oil is sometimes within the vary 2–3 because of the presence of carboxyl acids like acid and carboxylic acid.

The sturdy acidity will corrode pipe and burner parts. Measurements of the corrosiveness of bio-oil have shown that it will induce a lucid mass loss of steel and also the breakdown of a internal-combustion engine burner (Wright et al., 2010). recent bio-oil may be a homogenized liquid containing an exact quantity of solid particles. when long-run storage, it should separate into 2 layers and serious parts is also deposited at all-time low. As mentioned on top of, the high content of gas and volatile organic compounds are contributory to the ageing issues of bio-oil. The organic compound condensation of aldehydes and alcohols and self-aggregation of aldehydes to oligomers are 2 of the foremost doubtless reactions to require place. Coke and inorganic parts within the bio-oil can also have a chemical action impact, thereby enhancing the ageing method (Rick & Vix, 1991).

The aerated compounds in bio-oil will cause many issues in its direct combustion, like instability, low heating worth, and high corrosiveness. though higher water content will improve the flow properties and cut back Nox emissions within the fuel combustion method, it causes more issues. It not solely decreases the heating worth of the fuel, however additionally will increase the corrosion of the combustor and might lead to flame-out. The low hydrogen ion concentration worth of bio-oil additionally aggravates corrosiveness issues, which can cause higher storage and transportation prices. several researchers have tested the combustion of bio-oil in gas boiler systems, diesel engines, and gas turbines (Czernik&Bridgwater, 2004). recent bio-oil from totally different feedstocks will usually reach stable combustion in a very boiler system. One downside, however, is that the problem of ignition. The high water content of bio-oil not solely decreases its heating worth, however additionally consumes an outsized quantity of heat of vaporization (Bridgwater&Cottam, 1992). Thus, the direct ignition of bio-oil in a very cold chamber isn't simple, associate degreed an external energy supply is required for ignition and pre-heating of the chamber. The combustion of bio-oil in diesel engines is tougher. Its long ignition delay time, short burn length, and lower peak heat unleash have restricted its combustion properties (Vitolo&Ghetti, 1994). Experiments using bio-oil in gas turbines have proven for the most part unsuccessful. The high consistency and high ash content of bio-oil lead to severe obstruction and attrition issues within the injection system. Moreover, acid within the bio-oil is harmful to the mechanical parts of the turbine. Bio-oil may be a mixture of the many organic chemicals, like carboxylic acid, turpentine, methanol, etc. several compounds in bio-oil ar vital chemicals, like phenols utilized in the resins trade, volatile organic acids wont to manufacture de-icers, levoglucosan, hydroxyacetaldehyde, and a few agents applied within the pharmaceutical, fibre, and fertiliser industries, further as flavourer agents for food product (Radlein, 1999).

Bio-oil can not be directly applied as a top-quality fuel thanks to its inferior properties, like high water and gas contents, acidity, and low heating worth. Thus, it's necessary to upgrade bio-oil to supply a top-quality liquid fuel which will be utilized in engines (Bridgwater, 1996; Czernik&Bridgwater, 2004; Mortensen et al., 2011). seeable of its molecular structure and practical teams, and exploitation existing chemical processes for reference, like hydrodesulfurization, chemical action cracking, and fossil fuel steam reforming, many generic bio-oil upgrading technologies are developed, together with chemical process, cracking, esterification, emulsification, and steam reforming. parts with unsaturated bonds, like aldehydes, ketones, and alkenyl compounds, influence the storage stability of bio-oil, and chemical process may be wont to improve its overall saturation (Yao et al., 2008). chemical process are able to do a degree of deoxygenation of regarding eightieth, and remodel bio-oil into high-quality liquid fuel (Venderbosch et al., 2010; Wildschut et al., 2009). This method needs a high of chemical element, that will increase each the quality and value of the operation. Alcohol radical, carbonyl, and carboxyl teams were simply hydrodeoxygenated, and phenol radical and ether teams were additionally reactive, whereas furans, having a cyclic structure, were harder to convert (Furimsky, 2000). when the separation of bio-oil, the parts with alcohol radical, carbonyl, carboxyl, phenol radical, and ether teams is expeditiously hydrodeoxygenated at an occasional chemical element pressure, whereas the hydrodeoxygenation of a lot of complicated parts, like ethers and furans, is also achieved by developing special catalysts.

Catalytic cracking of bio-oil refers to the reaction whereby gas is removed within the style of CO, CO₂, and H₂O, within the presence of a solid acid catalyst, like water softener, yielding a hydrocarbon-rich top-quality liquid fuel. within the method of cracking, aerated compounds in bio-oil ar thought to endure initial deoxygenation to create light-weight olefins, that ar then cyclized to create aromatics or endure another reactions to supply hydrocarbons (Adjaye&Bakhshi, 1995a). Since bio-oil contains a

comparatively low H/C quantitative relation, and dehydration is amid the loss of chemical element, the H/C quantitative relation of the ultimate product is mostly low, and carbon deposits with massive aromatic structures tend to be shaped, which might cause deactivation of the catalyst (Guo et al., 2009a). The cracking of crude bio-oil is often terminated in a very short time, with a coke yield of regarding two hundredth (Adjaye&Bakhshi, 1995b; Vitolo et al., 1999). Alcohols, ketones, and carboxyl acids are expeditiously born-again into aromatic hydrocarbons, whereas aldehydes tend to condense to create carbon deposits (Gayubo et al., 2004b). Phenols additionally show low reactivity and coking happens promptly (Gayubo et al., 2004a). Besides, some thermally sensitive compounds, like pyrolytic polymer, may endure aggregation to create a precipitate, which might block the reactor and cause deactivation of the catalyst. Consequently, efforts are created to avoid this development by separating these compounds through thermal pre-treatment (Valle et al., 2010). Therefore, to keep up the steadiness and high performance of the cracking method, it's necessary to get fractions appropriate for cracking by separation of bio-oil, to realize the partial conversion of bio-oil into organic compound fuels.

Bio-oil contains a high content of carboxyl acids, thus chemical action esterification is employed to neutralize these acids. Each solid acid and base catalysts show high activity for the conversion of carboxyl acids into the corresponding esters, and also the heating worth of the upgraded oil is thereby raised markedly (Zhang et al., 2006). Since this technique is a lot of appropriate for the transformation of carboxyl acids that represent a comparatively tiny proportion of crude bio-oil, associate degree organic compound fuel with a high heating worth is expected to be made from the esterification of a fraction enriched with carboxyl acids obtained from the separation. The emulsion fuel obtained from bio-oil and diesel is homogenized and stable, and might be burned in existing engines. Analysis on the assembly of emulsions from crude bio-oil and diesel recommended that the emulsion made was a lot of stable than crude bio-oil. Later tests of those emulsions in numerous diesel engines showed that thanks to the presence of carboxyl acids, the widget nozzle was unsound, and this corrosion was accelerated by the high-speed flow within the spray channels (Chiaramonti et al., 2003a; Chiaramonti et al., 2003b). Besides corrosion, the high water content of bio-oil can lower the heating worth of the emulsion as a fuel, and a few high mass parts like sugar oligomers and pyrolytic polymer can increase the density and cut back the volatility of the emulsion. Thus, it's useful to check the emulsification of the separated fractions that contain less water and fewer high mass parts.

Catalytic steam reforming of bio-oil is additionally a vital upgrading technology for changing it into chemical element. Analysis on the steam reforming of carboxylic acid and grain alcohol is currently relatively mature, with high conversion of reactants, chemical element yields, and stability of the catalysts (Hu, 2007). However, some aerated compounds in bio-oil show inferior reforming behavior. Phenol can not be utterly born-again even at a high steam-to-carbon quantitative relation, whereas m-cresol and aldohexose not solely show low reactivity, however also are simply coked (Constantinou et al., 2009; Hu, 2009). To boost the reforming method, some additional investigations of steam reforming supported different separating ways are required. Therefore, it's necessary to mix crude bio-oil utilization with these upgrading technologies. Taking advantage of economical bio-oil separation to realize the enrichment of compounds within the same family or the parts that are appropriate for a similar upgrading technique may be a vital strategy for the long run utilization of top-quality bio-oil.

Separation Technologies

Solvent extraction: The solvents for extraction embody water, ester, paraffins, ethers, ketones, and alkalescent solutions. In recent years, some special solvents, like critical CO₂, have additionally been used for extraction or different analysis. By choosing acceptable solvents for extraction of the specified product, sensible separation of bio-oil is achieved. Some researchers have used non-polar solvents for the first separation of bio-oil, like dissolvent and n-hexane, so proceeded to extract the solvent-insoluble

fraction with water; finally, the soluble and water-insoluble fractions were additionally extracted with inhalation general anesthetic and chloride, severally (Garcia-Perez et al., 2007; Oasmaa et al., 2003). Tons of organic solvents are consumed throughout the method. Considering the value of those solvents and also the problem of the recovery method, the operational prices are unacceptable that hinders its industrial enterprise.

Supercritical fluid extraction relies on {the totally different|the various} dissolving skills of critical solvents below different conditions. Critical fluid extraction at low temperatures contributes to preventing undesirable reactions of thermally sensitive parts. Researchers sometimes use CO₂ because the critical solvent. In a very critical CO₂ extraction, compounds of low polarity (aldehydes, ketones, phenols, etc.) are by selection extracted, whereas acids and water stay within the residue part (Cui et al., 2010).

Column chromatography: The principle of chromatography is that substances are separated supported their totally different sorption capabilities on a stationary part. In general, extremely polar molecules are simply adsorbable on a stationary part, whereas weak polar molecules aren't. Thus, the method of chromatography involves sorption, desorption, re-adsorption, and redesorption. Colloid is often used because the stationary part, associate degree eluent is chosen per the polarity of the parts. Paraffin eluents, like alkane series and pentane, are wont to separate open-chain compounds. Aromatic compounds are sometimes eluted with benzol or dissolvent. {some different|another} polar compounds are obtained by extraction with methyl alcohol or other polar solvents (Ertas & Alma, 2010; Onay et al., 2006; Putun et al., 1999).

Distillation: Distillation may be a common separating technology within the industry. This technique separates the parts in turn per their totally different volatilities, and it's essential for the separation of liquid mixtures. air pressure distillation, vacuum distillation, steam distillation, and a few different forms of distillation are applied in biooil separation. Thanks to its complicated composition, the boiling of bio-oil starts below one hundred °C below air pressure, so the distillation continues up to 250–280 °C, whereat 35–50% of residue is left (Czernik & Bridgwater, 2004). The thermal sensitivity of bio-oil limits the operational temperature of distillation. Seeable of the unacceptable results obtained by air pressure distillation, researchers have utilized vacuum distillation to lower the boiling points of parts, and bio-oil might thereby be separated at an occasional temperature. Characterization of the distilled organic fraction showed that it had a way higher quality than the crude bio-oil, containing very little water and fewer aerated compounds, and having the next heating worth. Steam distillation is performed by introducing steam into the distilling vessel, to heat the bio-oil and reduce its consistency, and eventually the volatile parts are expelled by the steam. In a very study combining steam distillation with reduced pressure distillation, bio-oil was 1st steam distilled to recover fourteen.9% of a volatile fraction. The recovered fraction was then additionally distilled by reduced pressure distillation to recover sixteen sub-fractions (Murwanashyaka et al., 2001). During this method, a syringol-containing fraction was separated and syringol with a purity of ninety two.3% was obtained. Thanks to its thermal sensitivity, it's tough to expeditiously separate bio-oil by typical distillation ways. Molecular distillation looks to supply a possible means that of realizing biooil separation, as a result of it's the benefits of low operational temperature, short heating time, and high separation potency.

Molecular distillation: There are forces between molecules, which might be either repulsive or engaging counting on unit spacing. Once molecules are approximate, the repulsion is dominant. Once molecules aren't terribly on the brink of one another, the forces acting between them are engaging in nature, and there ought to be no unit forces if the gap between molecules is extremely massive. Since the distances

between gas molecules are massive, the unit forces are negligible, except once molecules touch one another.

The molecular mean free path is reciprocally proportional to the pressure and also the sq. of the effective molecular diameter. Below sure conditions, that is, if the temperature and pressure are fastened, the mean free path may be a perform of the effective molecular diameter. Apparently, a smaller molecule contains a shorter mean free path than a bigger molecule. Moreover, molecular mean free path can increase with increasing temperature or decreasing pressure.

Molecules can move earlier once the liquid mixture is heated. Surface molecules can overcome unit forces and escape as gas molecules after they acquire adequate energy. With associate degree raised quantity of gas molecules on top of the liquid surface, some molecules can come back to the surface. Below sure conditions, the molecular motion can reach dynamic equilibrium, that is manifested as equilibrium on a macroscopical scale. Ancient distillation technology separates parts by variations in their boiling points. However, molecular distillation (or short-path distillation) is kind of totally different and exactly depends on the varied mean free methods of various substances. The gap between the cooling and heating surfaces is a smaller amount than the mean free path for a lightweight molecule, however bigger than that for a significant molecule. Therefore, the sunshine molecules escaping from the heating surface will simply reach the cooling surface and be condensed. The equilibrium is thereby broken, and also the light-weight molecules are ceaselessly discharged from the liquid part. On the contrary, the serious molecules aren't discharged and come back to the liquid part. During this means, the sunshine and serious molecules are effectively separated. Molecular distillation technology has been wide utilized in the chemical, pharmaceutical, and foodstuff industries, further as in research to concentrate and purify organic chemicals. It's a possible method for the separation of thermally unstable materials, taking into consideration that it solely takes a couple of seconds to complete the separation method. Bio-oil may be a complicated mixture of the many compounds with a good varies of boiling points. It is thermally sensitive and simply undergoes reactions like decomposition, chemical change, and natural action. In addition, most of the compounds are gift in low concentrations. Molecular distillation isn't restricted by these unfavorable properties and is appropriate for the separation of bio-oil to facilitate analysis and quantification of its constituent compounds.

Conclusion

The shift product of biomass, bio-oil contains chemical compounds that complicate the appliance and additionally the cost-effectiveness of analysis. Among the commercially vital parts of bio-oil are sugars and synthetic resin compounds. Each are tough to research thanks to the big range of variations which will occur and cause potential interferences with different parts of bio-oil. Varied chemical separation ways are mentioned on top of. The separated chemicals have totally different applications in food, agriculture and chemical industries.

References:

- [1] Oasmaa, A., Kuoppala, E. &Solantausta, Y. (2003). Fast pyrolysis of forestry residue. 2. Physicochemical composition of product liquid. *Energy & Fuels*, Vol.17, No.2, pp. 433-443.
- [2] Bridgwater, A.V. (2012). Review of fast pyrolysis of biomass and product upgrading. *Biomass and Bioenergy*, Vol.38, pp. 68-94.
- [3] Adjaye, J.D., Sharma, R.K. &Bakhshi, N.N. (1992). Characterization And Stability Analysis of Wood -Derived Bio-Oil. *Fuel Processing Technology*, Vol.31, No.3, pp. 241-256.
- [4] Wright, M.M., Satrio, J.A., Brown, R.C. 2010. Techno-Economic Analysis of Biomass Fast Pyrolysis to Transportation Fuels. NREL
- [5] Rick, F., Vix, U. 1991. Product standards for pyrolysis products for use as fuel in industrial firing plant. in: *Biomass pyrolysis liquids upgrading and utilization*, Elsevier applied science, pp. 177-218.
- [6] Czernik, S. &Bridgwater, A.V. (2004). Overview of applications of biomass fast pyrolysis oil. *Energy & Fuels*, Vol.18, No.2, pp. 590-598.

- [7] Bridgwater, A.V. & Cottam, M.L. (1992). Opportunities For Biomass Pyrolysis Liquids Production And Upgrading. *Energy & Fuels*, Vol.6, No.2, pp. 113-120.
- [8] Vitolo, S. & Ghetti, P. (1994). Physical And Combustion Characterization Of Pyrolytic Oils Derived From Biomass Material Upgraded By Catalytic-Hydrogenation. *Fuel*, Vol.73, No.11, pp. 1810-1812.
- [9] Radlein, D. 1999. *The production of Chemicals from Fast Pyrolysis Bio-oils. Fast Pyrolysis of Biomass: A handbook*. CPL Press, Newbury.
- [10] Bridgwater, A.V. (1996). Production of high grade fuels and chemicals from catalytic pyrolysis of biomass. *Catalysis Today*, Vol.29, No.1-4, pp. 285-295.
- [11] Czernik, S. & Bridgwater, A.V. (2004). Overview of applications of biomass fast pyrolysis oil. *Energy & Fuels*, Vol.18, No.2, pp. 590-598.
- [12] Yao, Y., Wang, S.R. & Luo, Z.Y. (2008). Experimental research on catalytic hydrogenation of light fraction of bio-oil. *Journal of Engineering Thermophysics*, Vol.29, No.4, pp. 715-719.
- [13] Venderbosch, R.H., Ardiyanti, A.R. & Wildschut, J. (2010). Stabilization of biomass-derived pyrolysis oils. *Journal of Chemical Technology and Biotechnology*, Vol.85, No.5, pp. 674-686.
- [14] Wildschut, J., Mahfud, F.H. & Venderbosch, R.H. (2009). Hydrotreatment of Fast Pyrolysis Oil Using Heterogeneous Noble-Metal Catalysts. *Industrial & Engineering Chemistry Research*, Vol.48, No. 23, pp. 10324-10334.
- [15] Furimsky, E. (2000). Catalytic hydrodeoxygenation. *Applied Catalysis A-General*, Vol.199, No.2, pp. 147-190.
- [16] Adjaye, J.D. & Bakhshi, N.N. (1995a). Catalytic Conversion Of A Biomass-Derived Oil To Fuels And Chemicals .1. Model-Compound Studies And Reaction Pathways. *Biomass & Bioenergy*, Vol.8, No. 3, pp. 131-149.
- [17] Vitolo, S., Seggiani, M. & Frediani, P. (1999). Catalytic upgrading of pyrolytic oils to fuel over different zeolites. *Fuel*, Vol.78, No.10, pp. 1147-1159,
- [18] Gayubo, A.G., Aguayo, A.T. & Atutxa, A. (2004a). Transformation of oxygenate components of biomass pyrolysis oil on a HZSM-5 zeolite. I. Alcohols and phenols. *Industrial & Engineering Chemistry Research*, Vol.43, No.11, pp. 2610-2618.
- [19] Gayubo, A.G., Aguayo, A.T. & Atutxa, A. (2004b). Transformation of oxygenate components of biomass pyrolysis oil on a HZSM-5 zeolite. II. Aldehydes, ketones, and acids. *Industrial & Engineering Chemistry Research*, Vol.43, No.11, pp. 2619-2626.
- [20] Valle, B., Gayubo, A.G. & Aguayo, A.T. (2010). Selective Production of Aromatics by Crude Bio-oil Valorization with a Nickel-Modified HZSM-5 Zeolite Catalyst. *Energy & Fuels*, Vol.24, pp. 2060-2070,
- [21] Chiaramonti, D., Bonini, A. & Fratini, E. (2003a). Development of emulsions from biomass pyrolysis liquid and diesel and their use in engines - Part 1: emulsion production. *Biomass & Bioenergy*, Vol.25, No.1, pp. 85-99.
- [22] Chiaramonti, D., Bonini, A. & Fratini, E. (2003b). Development of emulsions from biomass pyrolysis liquid and diesel and their use in engines - Part 2: tests in diesel engines. *Biomass & Bioenergy*, Vol.25, No.1, pp. 101-111,
- [23] Hu, X. & Lu, G.X. (2009). Investigation of the steam reforming of a series of model compounds derived from bio-oil for hydrogen production. *Applied Catalysis B-Environmental*, Vol.88, No.3-4, pp. 376-385
- [24] Constantinou, D.A., Fierro, J.L.G. & Efstathiou, A.M. (2009). The phenol steam reforming reaction towards H₂ production on natural calcite. *Applied Catalysis B-Environmental*, Vol.90, No.3-4, pp. 347-359.
- [25] Garcia-Perez, M., Chaala, A. & Pakdel, H. (2007). Characterization of bio-oils in chemical families. *Biomass & Bioenergy*, Vol.31, No.4, pp. 222-242,
- [26] Cui, H., Wang, J. & Wei, S. (2010). Supercritical CO₂ extraction of bio-oil. *Journal Of Shandong Unirersity Of Technology (Science And Technology)*, Vol.24, No.6, pp. 1-5, 10.
- [27] Ertas, M. & Alma, M.H. (2010). Pyrolysis of laurel (*Laurusnobilis* L.) extraction residues in a fixed-bed reactor: Characterization of bio-oil and bio-char. *Journal of Analytical and Applied Pyrolysis*, Vol.88, No.1, pp. 22-29.
- [28] Onay, O., Gaines, A.F. & Kockar, O.M. (2006). Comparison of the generation of oil by the extraction and the hydropyrolysis of biomass. *Fuel*, Vol.85, No.3, pp. 382-392.
- [29] Putun, A.E., Ozcan, A. & Putun, E. (1999). Pyrolysis of hazelnut shells in a fixed-bed tubular reactor: yields and structural analysis of bio-oil. *Journal of Analytical and Applied Pyrolysis*, Vol.52, No.1, pp. 33-49.